

ABSTRACT

A reformer for reacting fuel (12) and oxidant (16, 18, 20) into reformat (22). The reformer has an oxidizing zone (24), a reforming zone (26) and an injection and mixture forming zone between the oxidizing zone (24) and the reforming zone (26). A mixture of fuel (12) and oxidant (16, 18, 20) is delivered to the oxidizing zone (24) and is delivered at least in part to the reforming zone (26) following at least partial oxidation of the fuel (12). Fuel (14) and heat (28) can be supplied to the reforming zone (26) in a method for reacting fuel (12) and oxidant (16, 18, 20) into reformat.

REFORMER AND METHOD FOR CONVERTING FUEL

5 Reformer and method for converting fuel and oxidant into
reformate AND OXIDANT INTO REFORMATE

Background of the Invention

Field of the Invention

10 **[0001]** The invention relates to a reformer for converting fuel and oxidant into reformate, comprising an oxidation zone and a reforming zone, wherein a mixture of fuel and oxidant may be supplied to the oxidation zone, and the mixture may be supplied at least partially to the reforming zone upon an at least partial oxidation of the fuel.

Description of Related Art

20 **[0002]** The invention relates further to a method for converting fuel and oxidant into reformate in a reformer having an oxidation zone and a reforming zone, wherein a mixture of fuel and oxidant is supplied to the oxidation zone, the mixture being supplied at least partially to the reforming zone upon an at least partial oxidation of the fuel.

25 **[0003]** Generic reformers and generic methods provide numerous fields of application. In particular, they serve for supplying a fuel cell with a hydrogen-rich gas mixture, from which electric energy may be generated on the basis of electrochemical processes. Such fuel cells are employed, for example, in the automotive field as auxiliary power sources, so called APUs ("auxiliary power unit").

30 **[0004]** The reforming process for converting fuel and oxidant into reformate may proceed according to various concepts. For example, the catalytic reforming is known, in which part of the fuel is oxidized in an exothermic reaction. This catalytic reforming has the drawback of a high heat generation which may irreversibly harm the system components, in particular the catalytic converter.

35 **[0005]** Another possibility for generating reformate from hydrocarbons is the "steam-reforming". In this process, hydrocarbons are converted within an endothermic reaction into hydrogen by the aid of water vapor.

5 **[10006]** A combination of these both concepts, that is, the reforming on the basis of an exothermic reaction and the production of hydrogen by means of an endothermic reaction in which the energy for steam-reforming is extracted from the combustion of hydrocarbons, is called an autothermic reforming. Herein, the additional drawbacks arise that a possibility for supplying water has to be provided. High temperature gradients between the oxidation zone and the reforming zone constitute further problems in the 10 temperature management of the entire system.

15 **[10007]** An example ~~for~~ of a reformer having an oxidation unit which is separated from a reforming unit is given in German Patent Application DE 199 43 248 A1, which corresponds to U.S. Patent No. 6,613,466. Additionally, in U.S. Patent Application Publication 20050198899, a system is disclosed that has a reaction chamber which is suited for at least partially oxidizing the anode exhaust gas before it is supplied to the reformer. The at least partial oxidation of the anode exhaust gas increases the amount of water which is delivered into the reformer, by which the reforming efficiency is distinctly improved. Furthermore, the reformer has a reaction space to which fuel, the at least partially oxidized anode exhaust gas and the residual air remaining after at least partial oxidation can be supplied. In this way, the oxidized anode exhaust gas and the remaining residual air can, if necessary, be preheated by oxidation prior to being introduced into the reaction space of the reformer; this has a very advantageous effect on reforming in many cases.

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Summary of the Invention

30 **[10008]** The invention is based on the object to provide a reformer and a method for converting fuel and oxidant into reformate, in which the mentioned problems are overcome at least partially and in which, in particular, problems due to high temperatures and large temperature gradients do not occur, respectively.

35 **[10009]** This object is solved in accordance with the features of invention by fuel and heat being additionally supplied to the independent claims. reforming zone.

Advantageous embodiments of the invention are defined in the dependent claims.

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[10010] The invention is established beyond the generic reformer in that fuel may additionally be supplied to the reforming zone, and in that heat may be supplied to the reforming zone. The additionally supplied fuel thus forms

5 together with the exhaust gas from the oxidation zone, the starting gas mixture for the reforming process. Due to the mixing of the fuel with the exhaust gas, a small λ -value is provided (for example $\lambda = 0.4$), and an endothermic reforming reaction can take place by supplying heat.

10 10011 In this context, it is especially beneficial that heat from the exothermic oxidation within the oxidation zone may be supplied to the reforming zone. The heat energy resulting from the oxidation zone is thus converted in the course of the reforming reaction such that the net heat generation of the entire process does not lead to problems in the temperature management of the reformer.

15 10012 Advantageously, it is provided that the reforming zone comprises an oxidation supply through which oxidant may be additionally supplied. In this manner, a further parameter for influencing the reforming is provided, in order to optimize it.

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25 10013 The invention is, in a very beneficial manner, further developed in that the additional fuel may be supplied to an injection and mixture forming zone and in that the additional fuel can flow from the injection and mixture forming zone into the reforming zone. This injection and mixture forming zone is thus arranged upstream of the reforming zone such that the reforming zone is provided with a well mixed starting gas for the reforming reaction.

30 10014 In this context, it is especially beneficial that the additional fuel is at least partially evaporated by the thermal energy of the gas mixture exiting the oxidation zone. Thus, the reaction heat from the oxidation may be utilized in a beneficial manner also for the evaporation process of the fuel.

35 10015 Further, it may be beneficial that the gas mixture generated in the oxidation zone may be partially supplied to the reforming zone, bypassing the injection and mixture forming zone. Thereby, a further possibility for influencing the reforming process is provided such that a further improvement of the reformate exiting the reformer can be achieved with regards to its usage.

5 10016 The invention is established beyond the generic method in that additional fuel is supplied to the reforming zone, and in that heat is supplied to the reforming zone. In this manner, the advantages and special characteristics of the reformer according to the present invention are achieved also in the course of a method. This also applies for the following especially preferred embodiments of the method according to the present invention.

10 10017 This method is beneficially further developed in that heat from the exothermic oxidation within the oxidation zone is supplied to the reforming zone.

15 10018 Further, it may be beneficial that the reforming zone comprises an oxidant supply through which additional oxidant is supplied.

20 10019 Within the scope of the method, it is preferred that the additional fuel is supplied to an injection and mixture forming zone and that the additional fuel flows from the injection and mixture forming zone into the reforming zone.

25 10020 In relation to the method, it is beneficially envisaged that the additional fuel is evaporated at least partially by the thermal energy of the gas mixture exiting the oxidation zone.

30 10021 Further, it can be provided that the gas mixture which is produced in the oxidation zone is partially supplied to the reforming zone, bypassing the injection and mixture forming zone.

35 10022 The invention is based on the conclusion that, by separating the oxidation zone and the reforming zone, and by mixing the exhaust gas from the oxidation zone with the additionally supplied fuel, a gas mixture may be produced which provides good preconditions with regards to the following reforming and/or which can be optimized by the further supply of exhaust gas and oxidant with regards to 40 the reforming process.

10023 The invention is now explained by way of example referring to the accompanying drawings and the preferred embodiments.

The drawings show in Brief Description of the Drawings

100241 Figure 1—is a schematic diagram of a reformer according to the present invention; and in

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100251 Figure 2—is a flow chart for explaining a method according to the present invention.

Detailed Description of the Invention

10 100261 Figure 1 shows a schematic diagram of a reformer 10 according to the present invention. Fuel to which fuel 12 and oxidant 16 can be supplied to the reformer 10 through from respective supplies. For the fuel 12, for example, diesel fuel may be considered, and the oxidant 16 is usually air. The reaction heat generated instantaneous within the initial combustion may be partially discharged in an optionally provided cooling zone 36. The mixture then further proceeds into the oxidation zone 24 which can be realized as a pipe which is arranged within the reforming zone 26. In alternative embodiments, the oxidation zone is realized by multiple pipes or a specific pipe arrangement within the reforming zone 26. Within the oxidation zone, a conversion of fuel and oxidant within an exothermic reaction having $\lambda \approx 1$ takes place. The gas mixture 32 produced thereby then enters an injection and mixture forming zone 30 in which it is mixed with injected fuel 14. The thermal energy of the gas mixture 32 can thereby support the evaporation of the fuel 14. Additionally, it can be provided that oxidant is supplied into the injection and mixture forming zone 30. The thus formed mixture then enters the reforming zone 26 where it is converted in an endothermic reaction, with, for example, $\lambda \approx 0.4$. The heat 28 needed for the endothermic reaction is discharged from the oxidation zone 24. For optimizing the reforming process, oxidant 18 may be additionally supplied into the reforming zone 26. Further, it is possible to directly supply part of the gas mixture 34 which is produced in the oxidation zone 24 to the reforming zone 26, bypassing the injection and mixture forming zone 30. The reformate 22 then flows out of the reforming zone 26 and is available for further utilization.

45 100271 Figure 2 shows a flow chart for explaining a method according to the present invention. In step S01, fuel and oxidant is supplied to an oxidation zone. Thereafter, in step S02, an at least partial oxidation of the fuel occurs.

According to step S03, the gas mixture exiting the oxidation zone is supplied to the injection and gas mixture forming zone. Further, in step S04, additional fuel is supplied to the injection and gas mixture forming zone. The mixture produced in the injection and mixture forming zone is then supplied in step S05 to the reforming zone, where it is reformed in step S06 within an endothermic reaction, utilizing the reaction heat of the exothermic oxidation. In step S07, the reformat is extracted.

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100281 The features of the present invention disclosed in the preceding description, in and the drawings and in the claims can be essential utilized for the implementation of the invention, individually and in combination.

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Reference numerals:

12 — fuel

14 — fuel

20 16 — oxidant

18 — oxidant

20 — oxidant

22 — reformat

24 — oxidation zone

25 26 — reforming zone

28 — heat

30 — injection and mixture forming zone

34 — gas mixture

36 — cooling zone

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